

## Supporting Information

### Direct Synthesis of Long-Chain Primary Alcohols from Syngas over Na-driven Co<sub>2</sub>C-Co Catalyst

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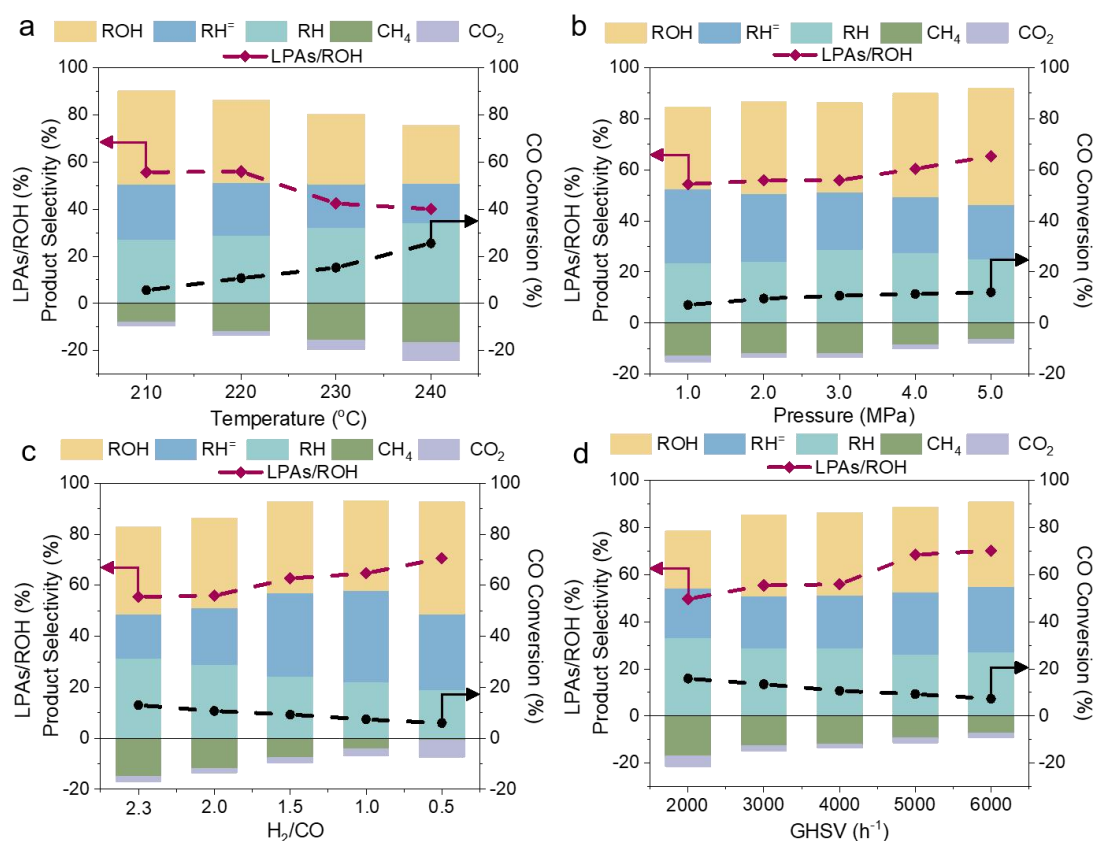
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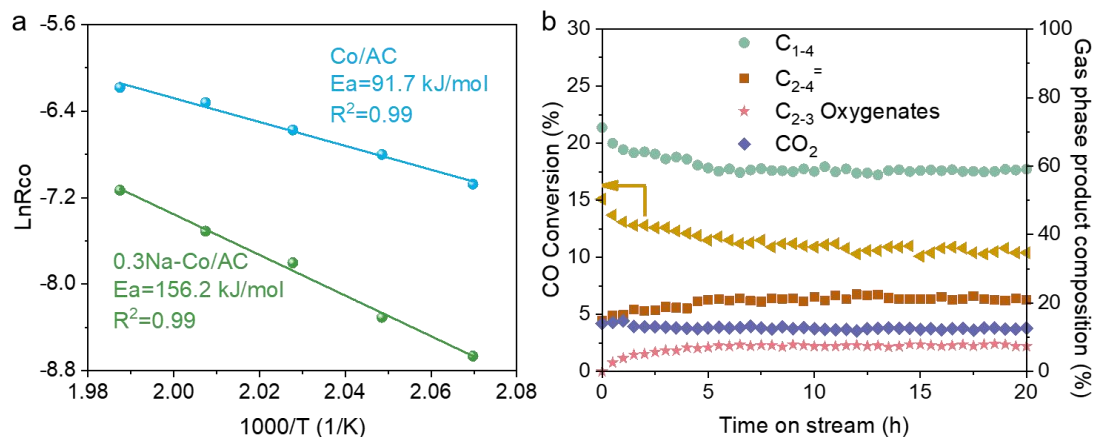
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**Figure S1.** The effect of reaction conditions on CO conversion and product selectivity over the 0.3Na-Co/AC catalyst (Figure S1a: 3.0 MPa, 4000 h<sup>-1</sup>, H<sub>2</sub>/CO = 2.0, and reaction temperature was ranged from 210 °C to 240 °C; Figure S1b: 220 °C, 4000 h<sup>-1</sup> H<sub>2</sub>/CO = 2.0, and reaction pressure was ranged from 1.0 MPa to 5.0 MPa; Figure S1c: 220 °C, 3.0 MPa, 4000 h<sup>-1</sup>, and H<sub>2</sub>/CO ratio was ranged from 0.5 to 2.3; Figure S1d: 220 °C, 3.0 MPa, H<sub>2</sub>/CO = 2.0, and GHSV was ranged from 2000 h<sup>-1</sup> to 6000 h<sup>-1</sup>).



**Figure S2.** Arrhenius plots for the calculation of the apparent activation energy ( $E_a$ ) over Co/AC and 0.3Na-Co/AC catalysts (a). CO conversion and gas phase product composition of 0.3Na-Co/AC catalyst in the initial stage of reaction (b), Reaction conditions: 220 °C, 3.0 MPa, 4000 h<sup>-1</sup> and H<sub>2</sub>/CO = 2.0.

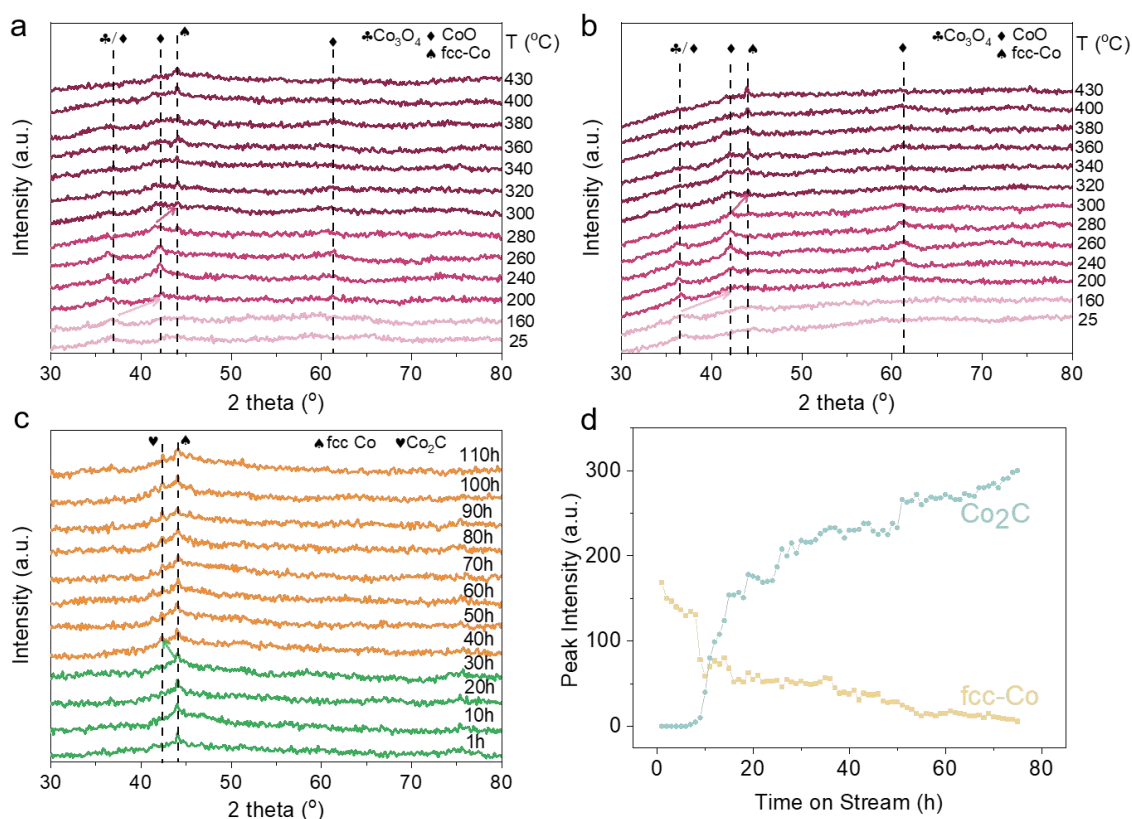
**Table S1.** The comparison of alcohol synthesis performance from syngas for representative catalysts

| Catalysts                                                                              | T (°C) | P (MPa) | GHSV (h <sup>-1</sup> ) | H <sub>2</sub> /CO ratio | X <sub>CO</sub> (%) | S <sub>CO2</sub> (%) | S <sub>CH4</sub> (%) | S <sub>ROH</sub> (%) <sup>b</sup> | S <sub>C6+OH</sub> (%) <sup>c</sup> | Ref       |
|----------------------------------------------------------------------------------------|--------|---------|-------------------------|--------------------------|---------------------|----------------------|----------------------|-----------------------------------|-------------------------------------|-----------|
| 0.3Na–Co <sub>2</sub> C–Co/AC                                                          | 220    | 5       | 4000                    | 2                        | 12.1                | 1.6                  | 6.3                  | 45.9                              | 30.0                                | This work |
| CoMn–0.6Na                                                                             | 240    | 2       | 6000 <sup>a</sup>       | 2                        | 11.6                | 31.6                 | 8.8                  | 19.8                              | 9.8                                 | [1]       |
| CuCoMn                                                                                 | 270    | 2.5     | 7500                    | 2                        | 29.7                | 0.4                  | 16.6                 | 46.2                              | 0.65 <sup>d</sup>                   | [2]       |
| Co/MnO <sub>x</sub> @quasi–MOF–74                                                      | 230    | 3       | 4500 <sup>a</sup>       | 2                        | 21.4                | 0.8                  | 10.0                 | 39.0                              | ~13.6                               | [3]       |
| CuCoAl                                                                                 | 270    | 2.5     | 7500                    | 2                        | 36.2                | 0.5                  | 24.0                 | 40.7                              | 0.65 <sup>d</sup>                   | [4]       |
| Co–Co <sub>2</sub> C/AC1                                                               | 200    | 3       | 3665 <sup>a</sup>       | 2                        | 71.4                | 7.6                  | –                    | 38.4                              | 15.0                                | [5]       |
| 15Co5Fe/AC                                                                             | 220    | 3       | 4000 <sup>a</sup>       | 2                        | 16.4                | 1.6                  | –                    | 20.6                              | 5.7                                 | [6]       |
| 15Co–0.5La/AC                                                                          | 220    | 3       | 1500                    | 2                        | 21.4                | 5.1                  | 23.8                 | 38.9                              | 13.3                                | [7]       |
| Co1Mn/AC                                                                               | 220    | 3       | 2000                    | 2                        | 29.1                | 2.4                  | 8.1                  | 21.4                              | ~8.6                                | [8]       |
| Co0.5Mn1La/AC                                                                          | 220    | 3       | 1000                    | 2                        | 32.2                | 3.2                  | 13.8                 | 25.7                              | ~5.1                                | [9]       |
| 15Co–0.1Ca/AC                                                                          | 220    | 3       | 900                     | 2                        | 49.0                | 0.7                  | –                    | 30.6                              | 16.1                                | [10]      |
| CuZnAl–A                                                                               | 250    | 4.5     | –                       | 2                        | 20.2                | 43.2                 | –                    | 27.0                              | ~0                                  | [11]      |
| CuZnFeMn                                                                               | 220    | 2       | 6000                    | 2                        | 23.5                | 6.9                  | –                    | 38.8                              | ~0.8                                | [12]      |
| Ca <sub>0.7</sub> La <sub>0.3</sub> Ti <sub>0.7</sub> Co <sub>0.3</sub> O <sub>3</sub> | 270    | 3       | 3900 <sup>a</sup>       | 2                        | 12.0                | ~7.0                 | –                    | 42.0                              | ~0                                  | [13]      |
| CoMnZn/r–TiO <sub>2</sub>                                                              | 260    | 4       | 2000 <sup>a</sup>       | 2                        | 44.7                | free                 | ~19                  | 43.4                              | ~17.4 <sup>d</sup>                  | [14]      |

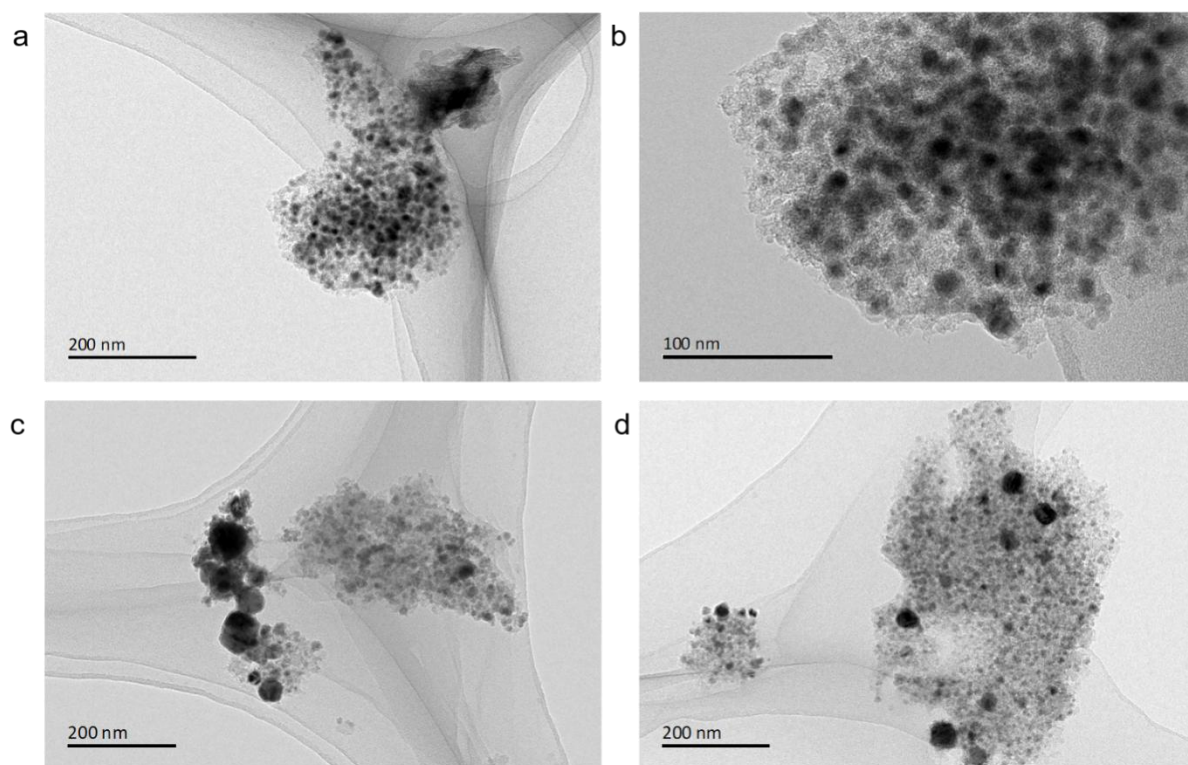
<sup>a</sup> WHSV: ml/g<sub>cat</sub>/h. <sup>b</sup> ROH (total alcohols). <sup>c</sup> Alcohols with six or more carbon numbers. <sup>d</sup> Alcohols with five or more carbon numbers.

**Table S2.** Textural properties of various catalysts determined by N<sub>2</sub> physical adsorption–desorption

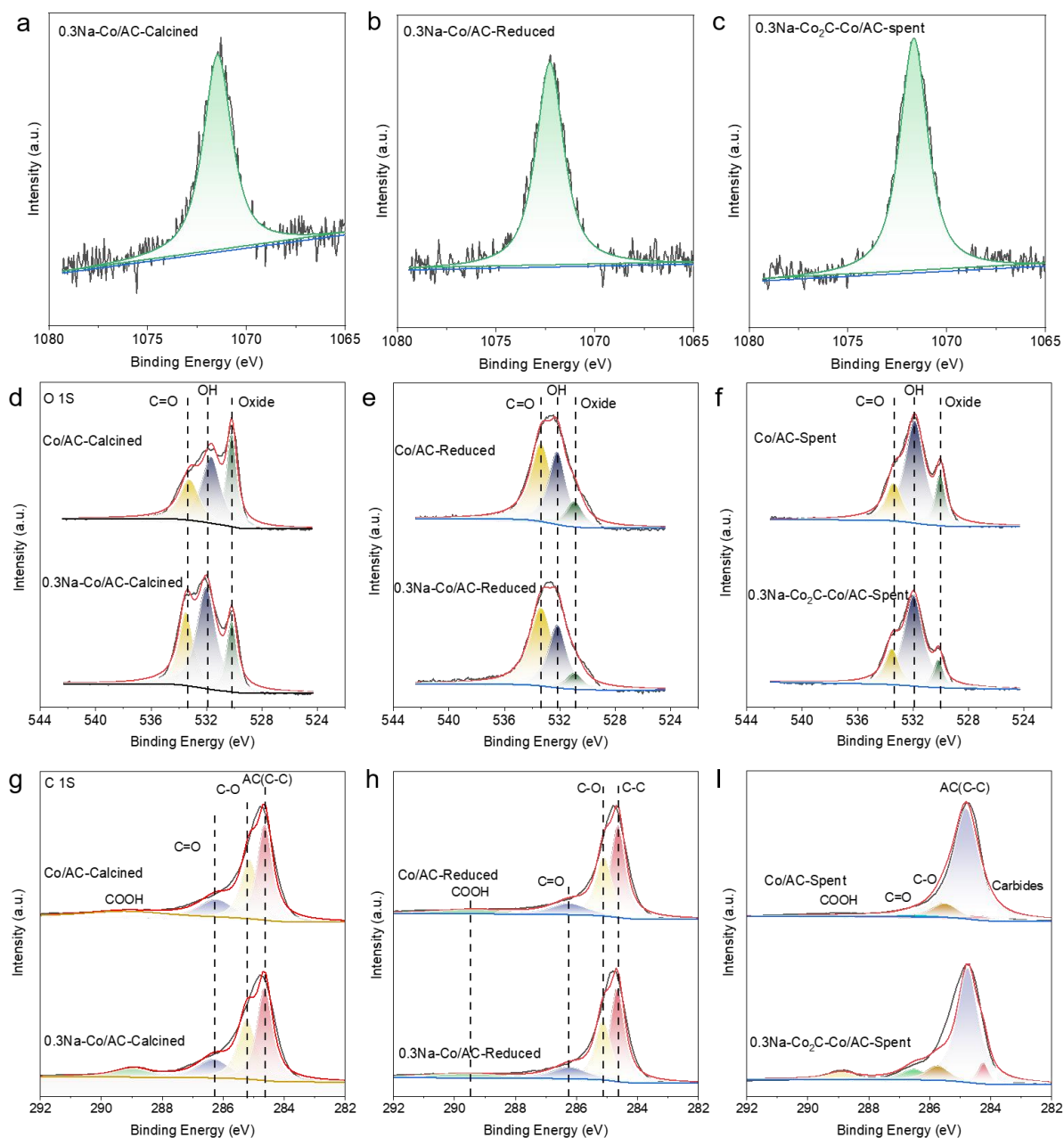
| Catalysts   | $A_{\text{BET}}$ (m <sup>2</sup> /g) | $V_{\text{total}}$ (cm <sup>3</sup> /g) | D (Å) |
|-------------|--------------------------------------|-----------------------------------------|-------|
| Co/AC       | 837                                  | 0.19                                    | 19.1  |
| 0.1Na–Co/AC | 808                                  | 0.19                                    | 19.2  |
| 0.3Na–Co/AC | 738                                  | 0.17                                    | 19.1  |
| 0.5Na–Co/AC | 665                                  | 0.12                                    | 19.1  |



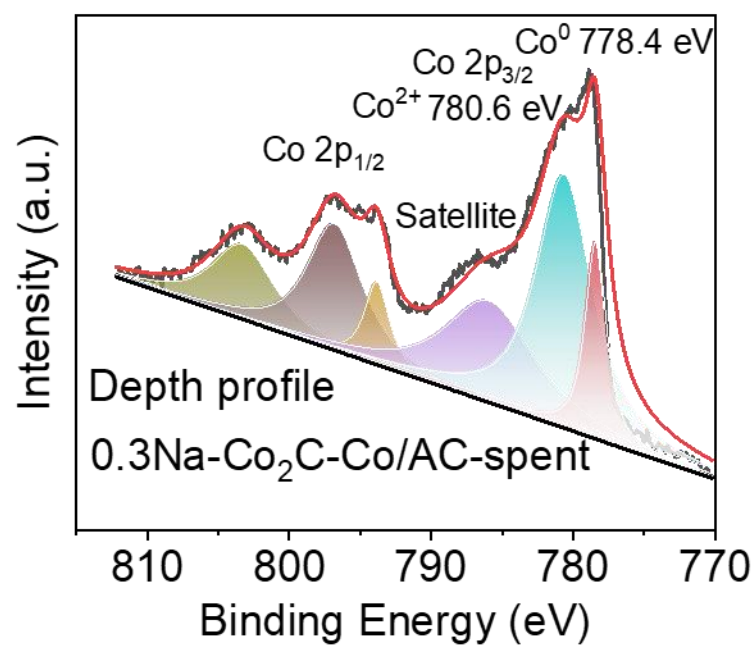
**Figure S3.** Temperature-programmed reduction of Co/AC (a) and 0.3Na-Co/AC (b) catalysts in a H<sub>2</sub> atmosphere, as well as temperature-programmed reactions of Co/AC catalysts in a syngas (H<sub>2</sub>/CO=2.0) atmosphere characterized by *in situ* XRD (c). Reaction-induced formation of Co<sub>2</sub>C promoted by Na as a function of time characterized by *in situ* XRD (d).



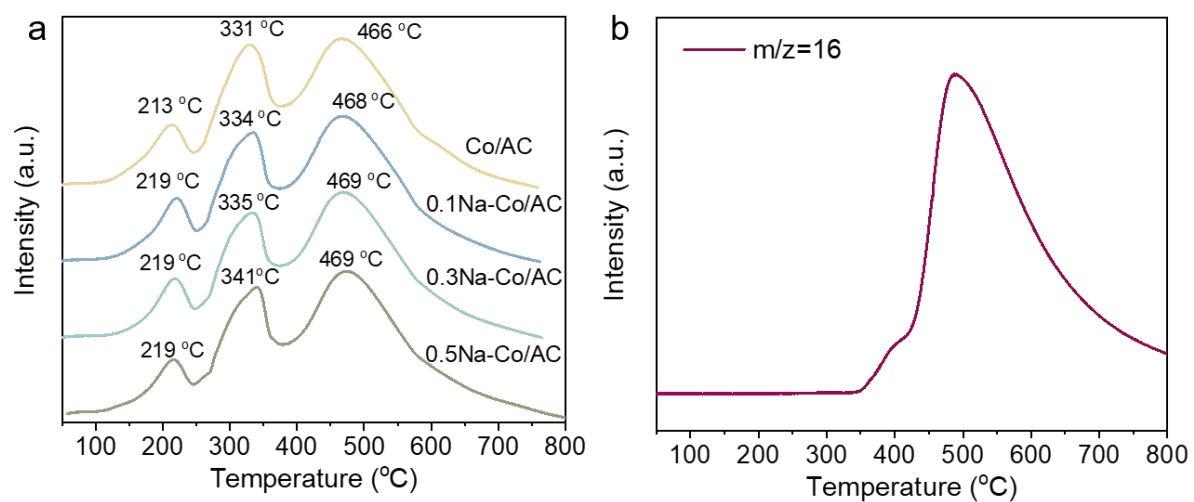
**Figure S4.** HRTEM images for spent 0.3Na–Co<sub>2</sub>C–Co/AC (a and b) and Co/AC (c and d) catalysts.



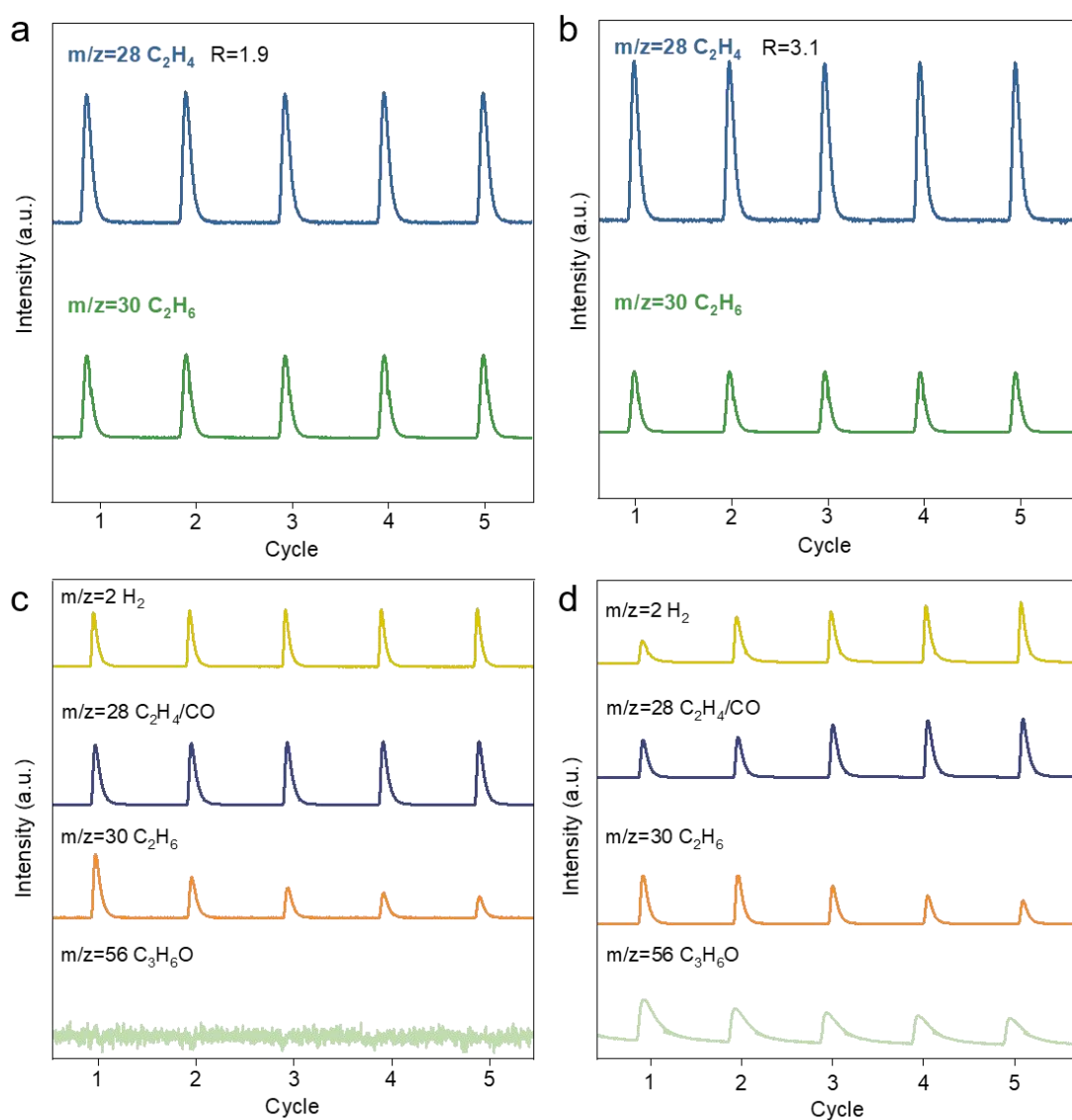
**Figure S5.** XPS spectra of Co/AC and 0.3Na-Co/AC catalysts under varying treatment conditions. Na 1s spectra: (a) Calcined at 350 °C in Ar atmosphere; (b) *In situ* reduced at 430 °C under H<sub>2</sub> for 4 h; (c) Spent after 48 h time on stream, at the condition of 220 °C, 3.0 MPa, GHSV = 4000 h<sup>-1</sup>, H<sub>2</sub>/CO = 2.0. O 1s spectra: (d) Calcined at 350 °C in Ar atmosphere; (e) *In situ* reduced at 430 °C under H<sub>2</sub> for 4 h; (f) Spent after 48 h time on stream, at the condition of 220 °C, 3.0 MPa, GHSV = 4000 h<sup>-1</sup>, H<sub>2</sub>/CO = 2.0. C 1s spectra: (g) Calcined at 350 °C in Ar atmosphere; (h) *In situ* reduced at 430 °C under H<sub>2</sub> for 4 h; (i) Spent after 48 h time on stream, at the condition of 220 °C, 3.0 MPa, GHSV = 4000 h<sup>-1</sup>, H<sub>2</sub>/CO = 2.0.



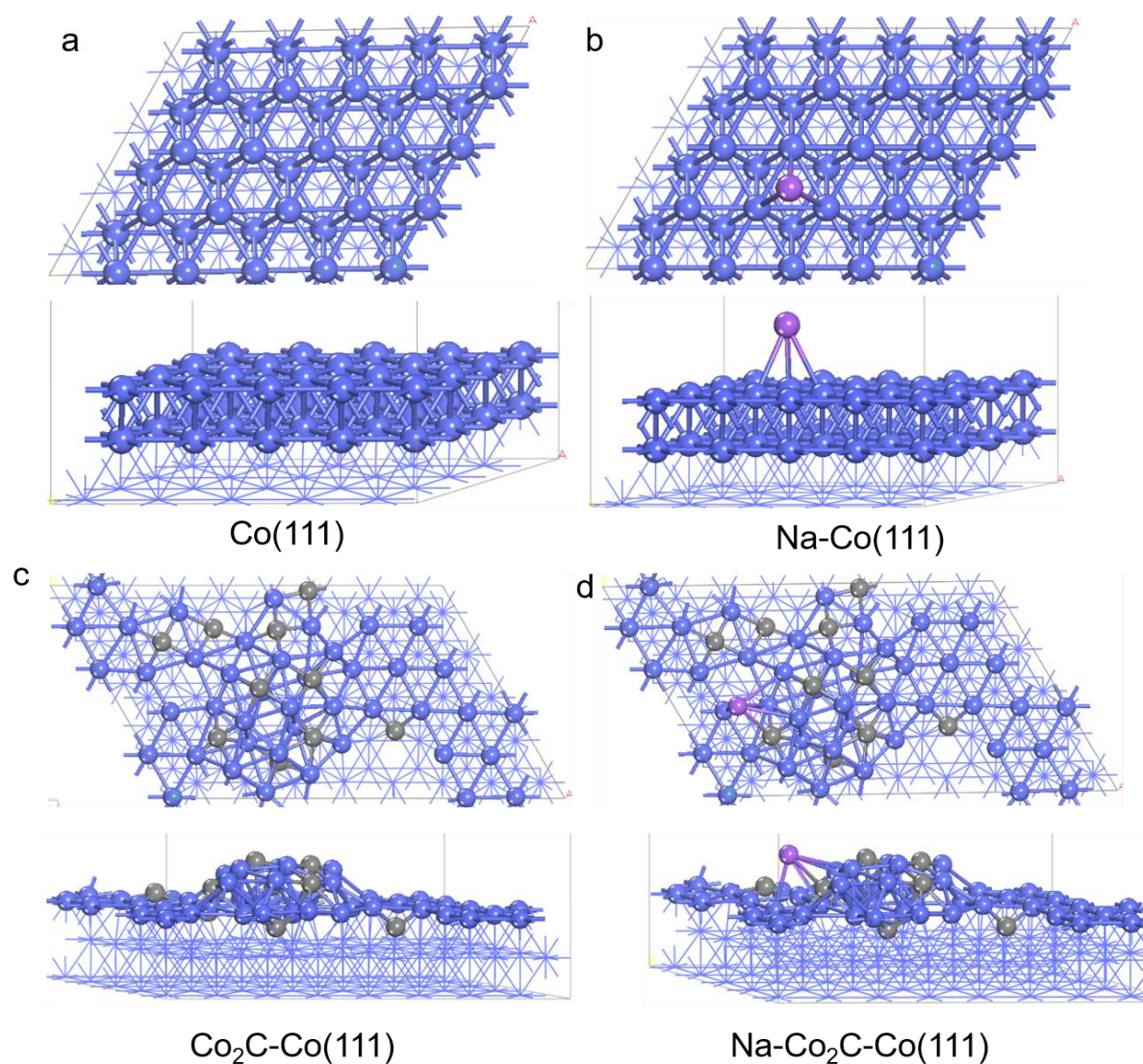
**Figure S6.** Depth-profiling Co 2p XPS spectra of 0.3Na–Co<sub>2</sub>C–Co/AC–spent catalysts.



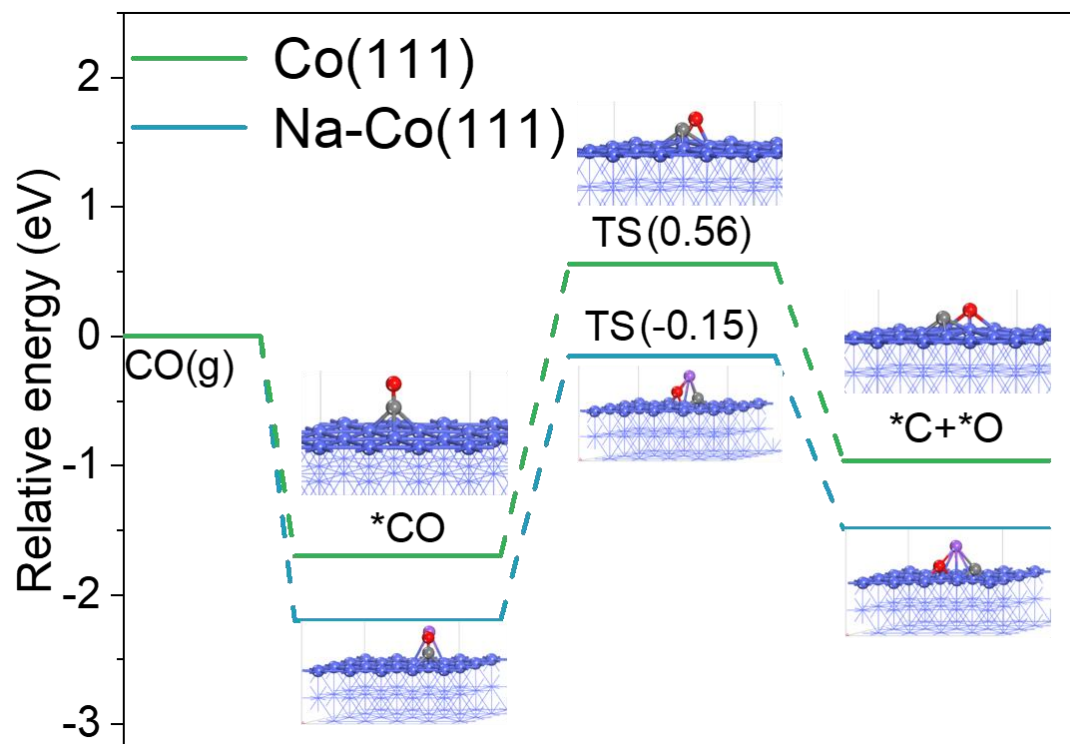
**Figure S7.**  $H_2$ -TPR profiles of the xNa-Co/AC catalysts (a) and  $H_2$ -TPR-MS ( $m/z=16$ ) profiles of the 0.3Na-Co/AC catalysts (b).



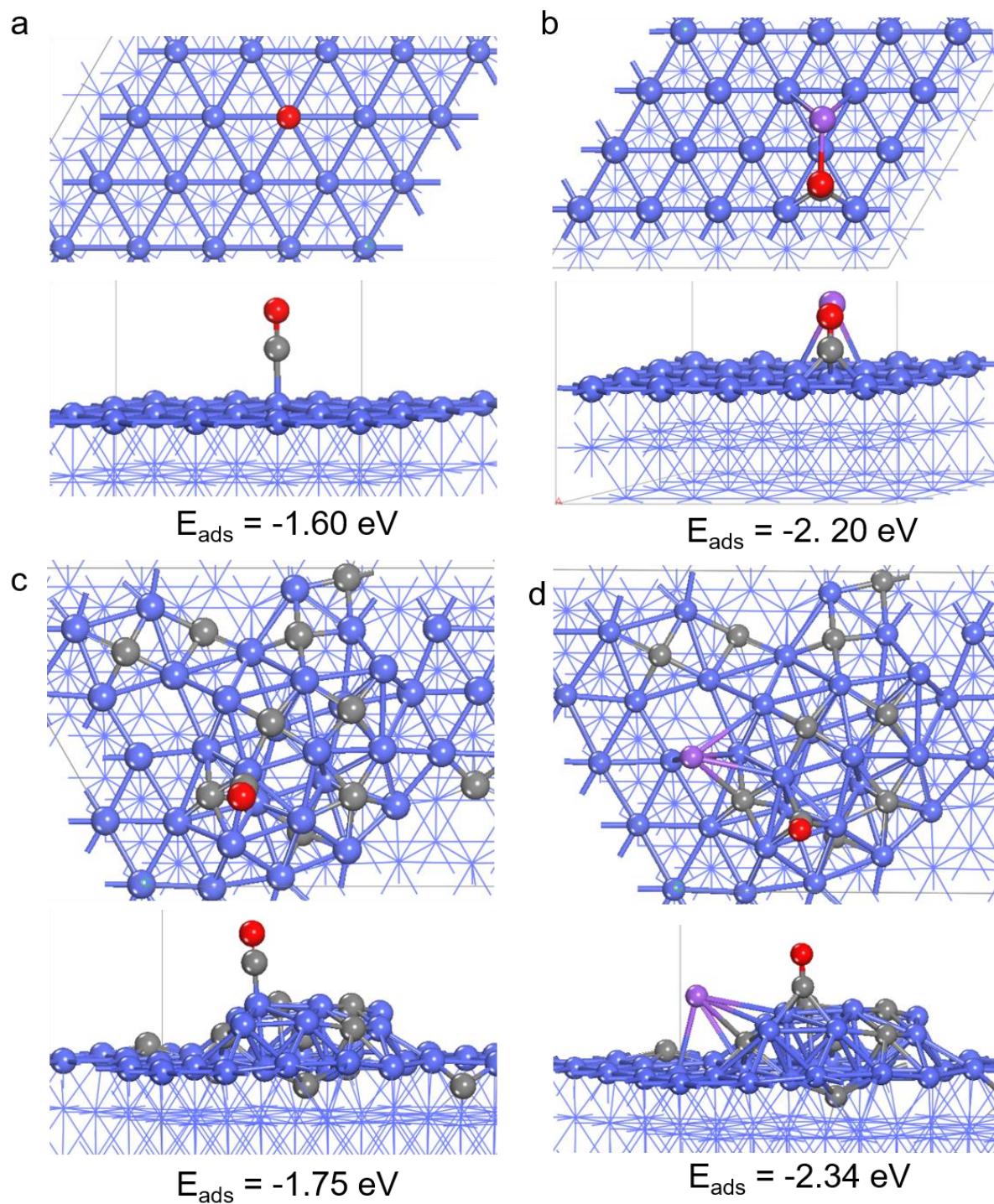
**Figure S8.** Transient response curves of ethylene hydrogenation pulse experiments at 220 °C over Co/AC (a) and 0.3Na-Co<sub>2</sub>C-Co/AC (b). Transient response curves from ethylene, carbon monoxide and hydrogen pulse experiments at 220 °C for Co/AC (c) and 0.3Na-Co<sub>2</sub>C-Co/AC (d).



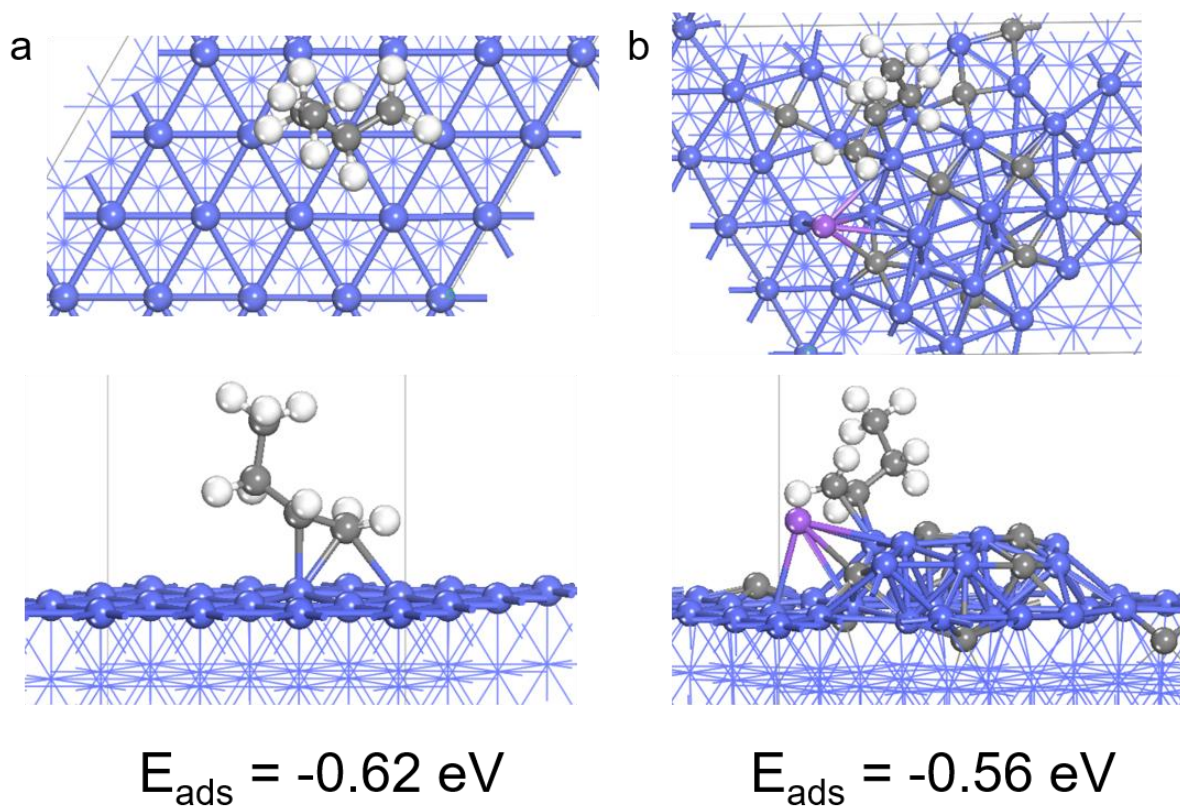
**Figure S9.** Illustrations of the top and side views of the surface of (a) Co (111), (b) Na–Co (111), (c) Co<sub>2</sub>C–Co (111) and Na–Co<sub>2</sub>C–Co (111). Color code: Co, blue; C, black; and Na, purple.



**Figure S10.** Schematic representation of the mechanisms for CO dissociation pathways on Co (111) and Na–Co (111) surfaces.



**Figure S11.** Illustrations of different configurations of CO\* adsorptions and their associated adsorption energy values on the (a) Co (111), (b) Na-Co (111), (c) Co<sub>2</sub>C-Co (111) and (d) Na-Co<sub>2</sub>C-Co (111) surfaces. Color code: Co, blue; C, black; O, red; and Na, purple.



**Figure S12.** Illustrations of different configurations of  $\text{*C}_4\text{H}_8$  adsorptions and their associated adsorption energy values on the (a) Co (111) and (b) Na–Co<sub>2</sub>C–Co (111) surfaces. Color code: Co, blue; C, black; H, white; and Na, purple.

## Reference

- [1] Y. Yang, T. Lin, X. Qi, F. Yu, Y. An, Z. Li, Y. Dai, L. Zhong, H. Wang, Y. Sun, *Appl. Catal. A Gen.*, **2018**, 549, 179–187.
- [2] K. Sun, M. Tan, Y. Bai, X. Gao, P. Wang, N. Gong, T. Zhang, G. Yang, Y. Tan, *J. Catal.*, **2019**, 378, 1–16.
- [3] W. Cui, Y. Li, H. Zhang, Z. Wei, B. Gao, J. Dai, T. Hu, *Appl. Catal. B: Environ.*, **2020**, 278, 119262.
- [4] K. Sun, Y. Wu, M. Tan, L. Wang, G. Yang, M. Zhang, W. Zhang, Y. Tan, *ChemCatChem*, **2019**, 11, 2695–2706.
- [5] Y. Pei, J. Liu, Y. Zhao, Y. Ding, T. Liu, W. Dong, H. Zhu, H. Su, L. Yan, J. Li, W. Li, *ACS Catal.*, **2015**, 5, 3620–3624.
- [6] H. Du, H. Zhu, Z. Zhao, W. Dong, W. Luo, W. Lu, M. Jiang, T. Liu, Y. Ding, *Appl. Catal. A Gen.*, **2016**, 523, 263–271.
- [7] G. Jiao, Y. Ding, H. Zhu, X. Li, J. Li, R. Lin, W. Dong, L. Gong, Y. Pei, Y. Lu, *Appl. Catal. A Gen.*, **2009**, 364, 137–142.
- [8] Z. Zhao, W. Lu, R. Yang, H. Zhu, W. Dong, F. Sun, Z. Jiang, Y. Lyu, T. Liu, H. Du, Y. Ding, *ACS Catal.*, **2018**, 8, 228–241.
- [9] Z. Zhao, W. Lu, H. Zhu, W. Dong, Y. Lyu, T. Liu, X. Chen, Y. Wang, Y. Ding, *J. Catal.*, **2018**, 361, 156–167.
- [10] H. Du, H. Zhu, X. Chen, W. Dong, W. Lu, W. Luo, M. Jiang, T. Liu, Y. Ding, *Fuel*, **2016**, 182, 42–49.
- [11] P. Luo, Y. Liu, K. Wang, Z. Li, C. Zhang, Y. Wu, X. Zan, W. Huang, *Fuel Process. Technol.*, **2023**, 245, 107728.
- [12] M. Lin, K. Fang, D. Li, Y. Sun, *Catal. Commun.*, **2008**, 9, 1869–1873.
- [13] P. Song, J. Wang, X. Wang, N. Li, Z. Zhang, Y. Liu, *Chem. Eng. J.*, **2022**, 439, 135635.
- [14] X. Qi, T. Lin, Y. An, X. Wang, D. Lv, Z. Tang, L. Zhong, *ACS Catal.*, **2023**, 13, 11566–11579.